

Unconventional systems for seaborne CO2 transportation systems

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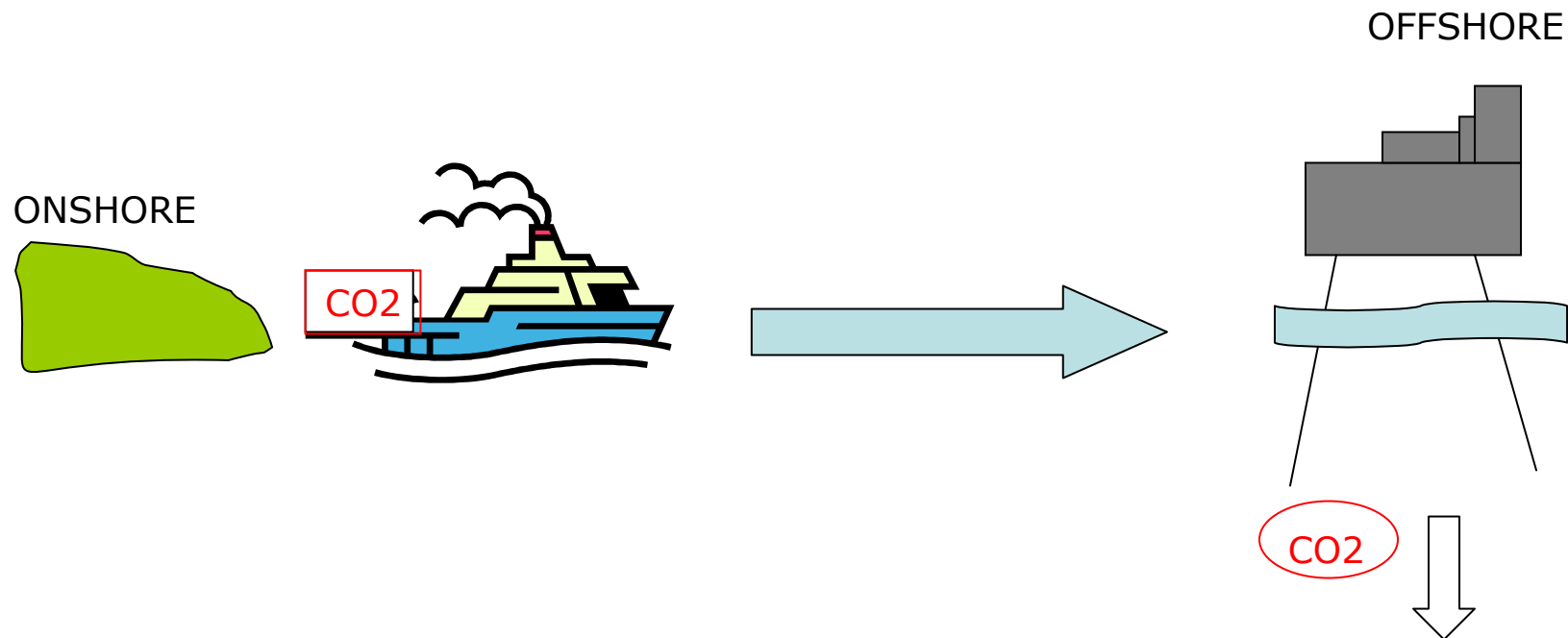
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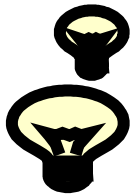
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This paper will compare 3 alternatives of CO₂ transported by ship from onshore to existing offshore platform.

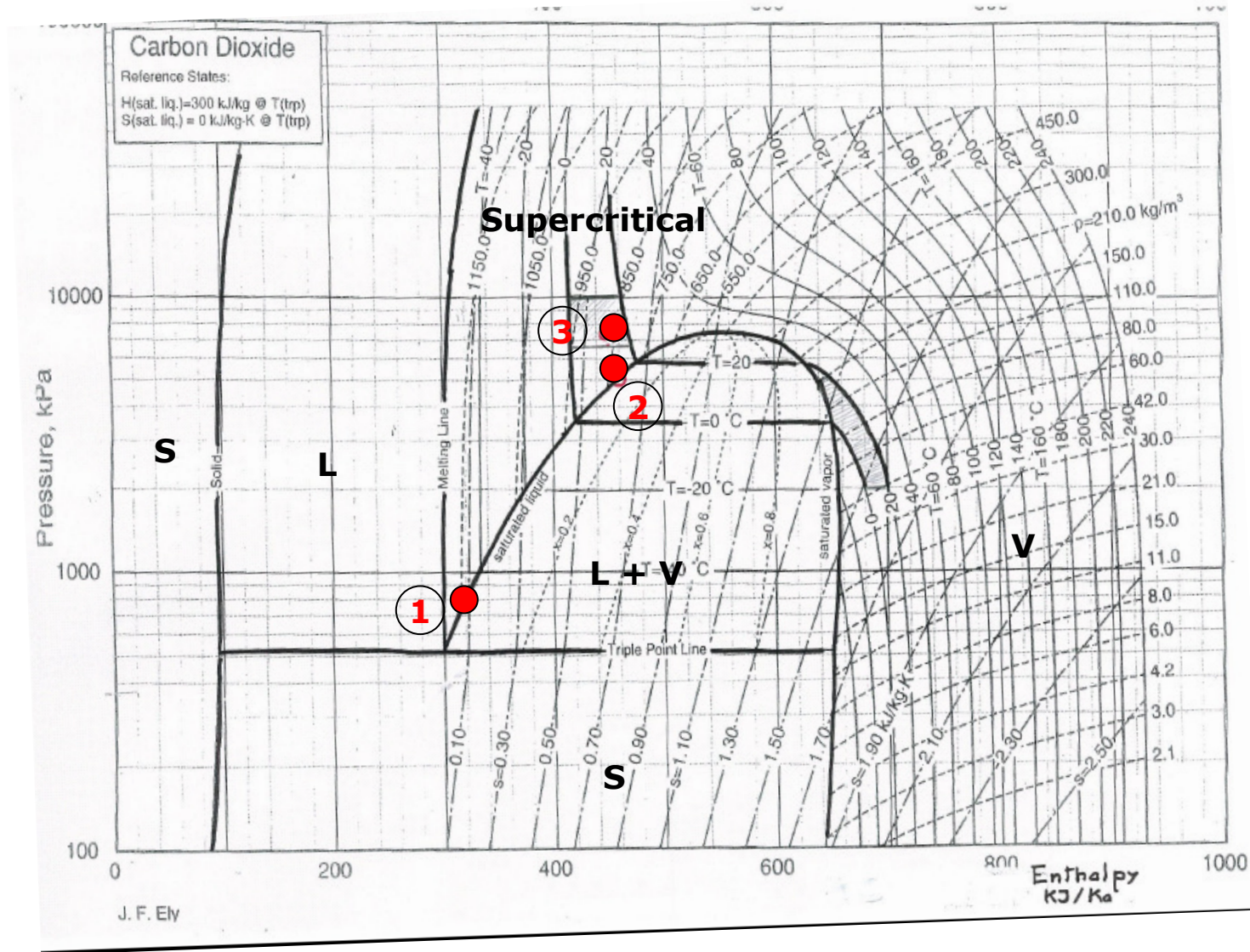


LOOK AT THE CO2 DIAGRAM AND CHARACTERISTICS



Case	type	Pressure/ temperature	Ship back to shore	Form
1	conventional	8 bar -46 ° C	empty	Liquid
2	unconventional	50 bar + 15° C	empty	Liquid
3	unconventional	75 bar + 15° C	with NG	Supercritical

SIMPLIFIED DIAGRAM OF CO2



Case 1

Transport is made on liquid refrigerated form, pressure about 8 bars, temperature – 46° C

- Pressure should be selected to avoid plugging in solid under transitional pressure loss in piping (higher than triple point)
- Containment more difficult than LPG as combining both pressure and cold
- Thickness limitations for spheres

CONVENTIONAL SIMPLIFIED SCHEME (Case 1)

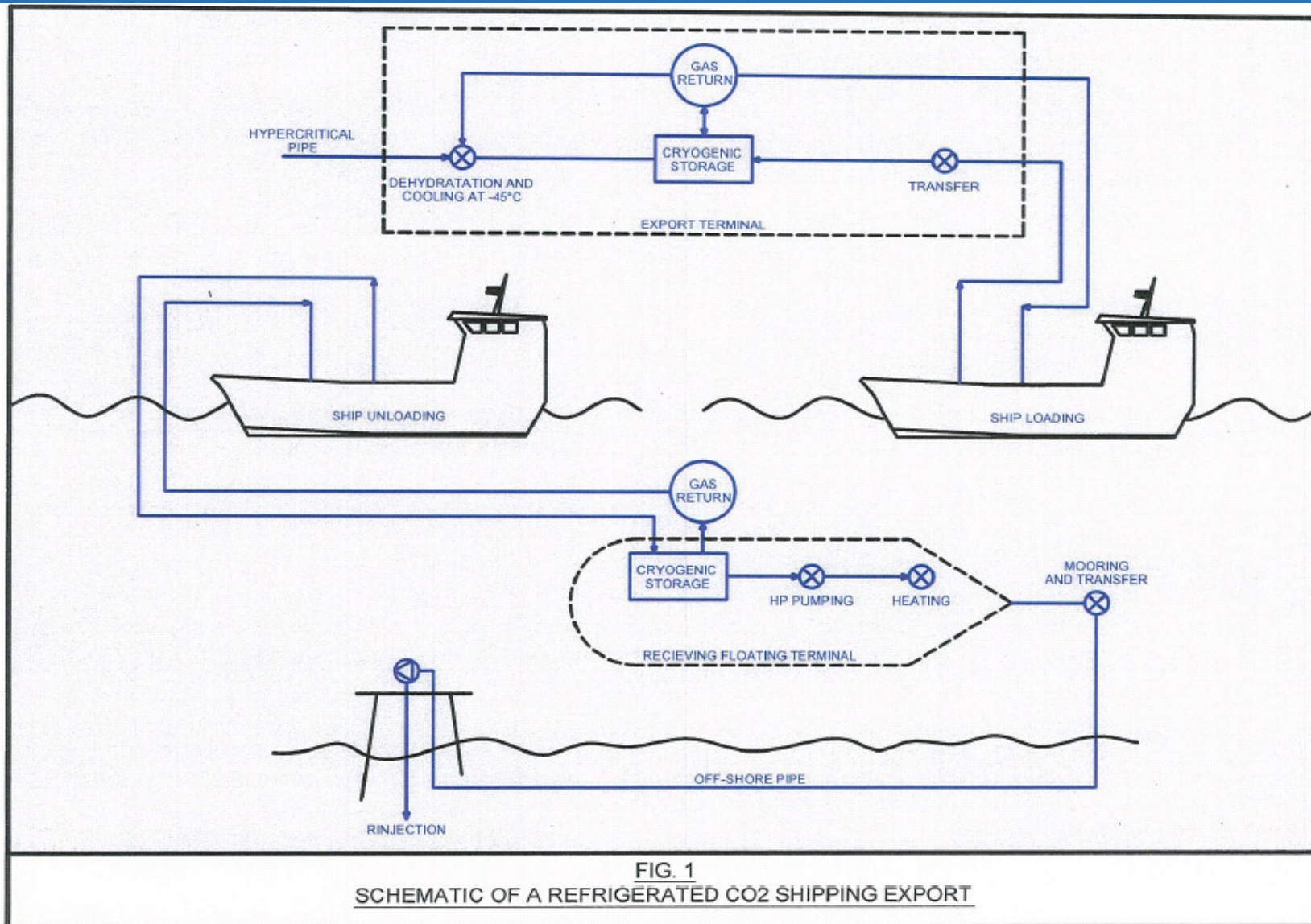


FIG. 1
SCHEMATIC OF A REFRIGERATED CO2 SHIPPING EXPORT

Investment (CAPEX)

export terminal	379 MM\$
6 ships (6 x 129 MM\$)	774 MM\$
receiving offshore facilities	220 MM\$
Total investment	1,373 MM\$

CAPEX/year (7.5%/15 years) 155.6 MM\$/y

OPEX

export terminal	37.9 MM\$/y
6 ships (6 x 16.3 MM\$)	97.8 MM\$/y
receiving offshore facilities	22.0 MM\$/y
Total OPEX	157.7 MM\$/y
Total CAPEX + OPEX	313.3 MM\$/y

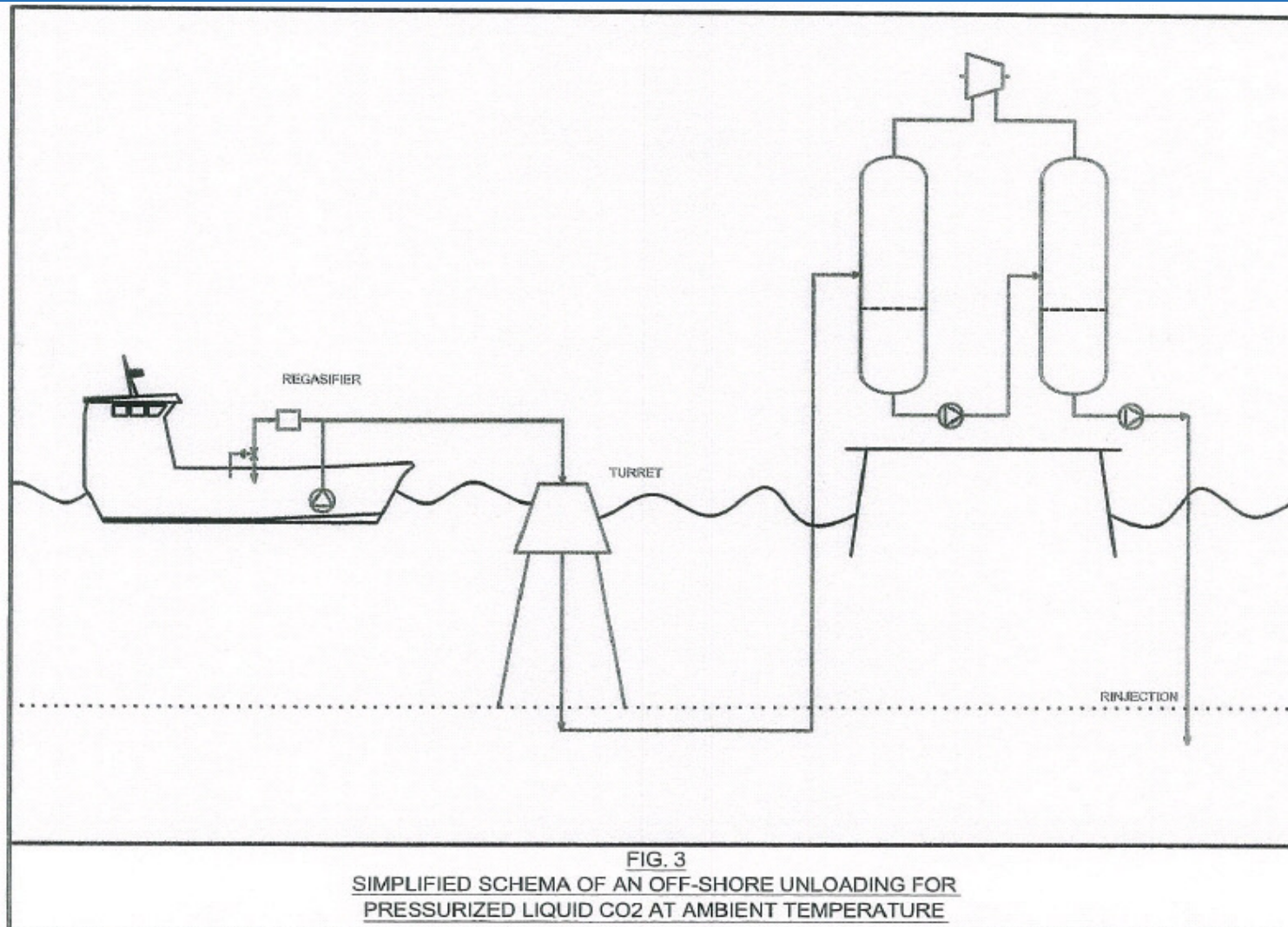
Unit cost	26.1 \$/t
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UNCONVENTIONAL SOLUTIONS CONSIDERED
CARBOTUBE (patented P92943EPOO by MET) –
Cases 2 & 3



- Ambient temperature, under pressure
- Containment made with current pipes used in gas line
 - More weight than sphere
 - Less unit cost per kg
- Two solutions:
 - Liquid at 15° C, 50 bars → **Case 2**
 - Supercritical at 15° C, 75 bars → **Case 3**
- Shuttle type of shipping operation to minimize terminal facilities

SIMPLIFIED SCHEME FOR RECEIVING FACILITIES (Case 2)



Investment (CAPEX)

export terminal	100 MM\$
ships (8 x 123 MM\$)	984 MM\$
receiving offshore facilities	90 MM\$

Total investment **1,174 MM\$**

CAPEX/year (11.33%) **133 MM\$/y**

OPEX

export terminal	37.9 MM\$/y
ships (8 x 17.9 MM\$)	97.8 MM\$/y
receiving offshore facilities	22.0 MM\$/y
Total OPEX	162.2 MM\$/y

Total investment (CAPEX + OPEX) **295.2 MM\$/y**

Unit cost	24.6 \$/t
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Case 3

- CO₂ is transported at 75 bars / 15° C
- Containment is based on linear tubular gas line pipe modules connected in series
- Transfer is obtained by exchange with natural gas under slight differential pressure, assumed to be available on reinjection site or nearby
- Natural gas is delivered on the way back to export terminal, displaced by CO₂ loaded

Two possible containments

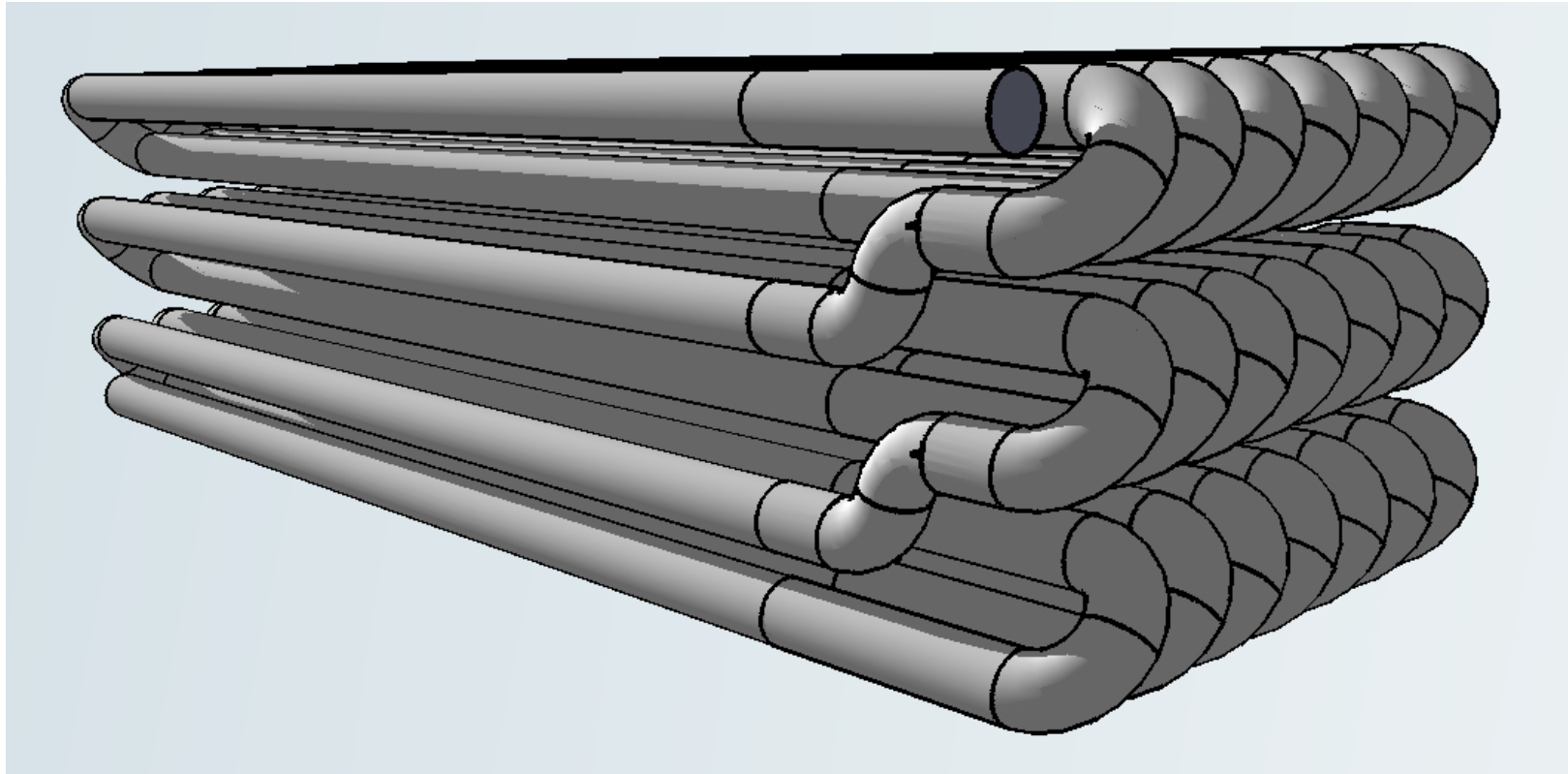
A. Horizontal tubular containment

- Bundle of 28" pipes (quadruple jointing) 12.7 mm
 - Size of one bundle module 6.8 x 7.8 x 51 m
- | | | | |
|-----------------|----------|-------|---------|
| weight of steel | pipes | 529 t | } 633 t |
| | fittings | 24 t | |
| | frame | 80 t | |
- Content of CO₂ 746 t

B. "COSELLE" type with 8" coiled

- Typical size of one coselle diameter 19 m / height 5 m
12,800 m of coiled 8" pipe
- Weight (320 + 50) 370 t
- Content of CO₂ 375 t 375 t

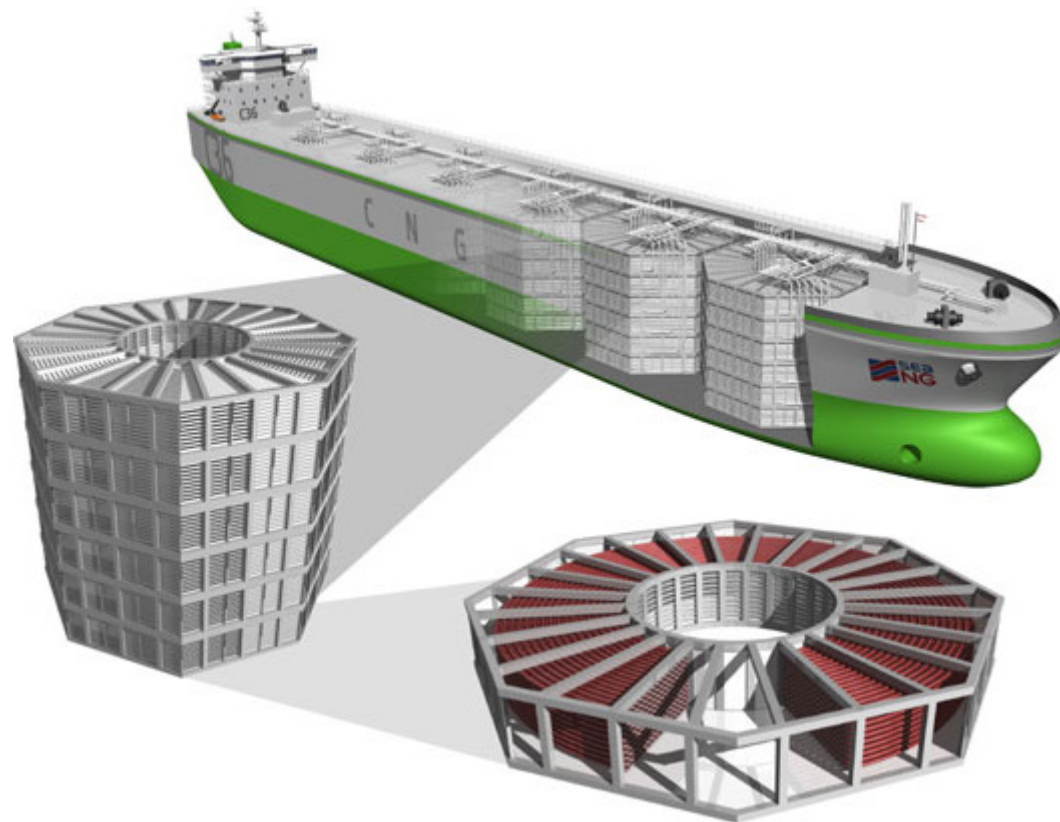
FIGURE OF ONE HORIZONTAL BUNDLE MODULE (Case 3)



Typically one bundle will be like a 2,500 m fold-up pipeline, and the 16 modules installed in one ship compartment a 40-km fold-up pipeline

Interface will then move at less than 0.5 m/s

FIGURE OF ONE COSELLE (Case 3)



ECONOMICS

12 MTPA (supercritical 75 bars) – Case 3



Investment (CAPEX)

export terminal	75 MM\$
ships (8 x 148 MM\$)	1,184 MM\$
receiving offshore facilities	70 MM\$

Total investment **1,329 MM\$**

CAPEX/year (11.33%) **150.5 MM\$/y**

OPEX

export terminal	10 MM\$/y
ships (8 x 17.9 MM\$)	143.2 MM\$/y
receiving offshore facilities	7 MM\$/y

Total OPEX **162.5 MM\$/y**

CAPEX + OPEX **313 MM\$/y**

Less added value of gas (5 \$MMbtu)

846 t of gas x 250 \$/t **- 211 MM\$/y**

Total/year **102 MM\$/y**

Unit cost

8.51 \$/t

SUMMARY OF COMPARISON



		Case 1	Case 2	Case 3
		8 bar -46° C	50 bar +15° C	75 bars +15° C
Item designation	units	Refrigerated solution	Ambient pressurized	Ambient supercritical + GN return
Investment				
- export terminal	MM \$	379	100	75
- ships (number)	MM \$	774 (6)	984 (8)	1,184 (8)
- receiving off-shore	MM \$	90	90	70
Total investment	MM \$	1,373	1,174	1,329
OPEX				
- export terminal	MM \$/y	37.9	10	7.5
- ships (number)	MM \$/y	97.8	143.2	148
- receiving off-shore	MM \$/y	22	9	7
Total OPEX	MM \$/y	157.7	162.2	162.5
BALANCE / YEAR				
- CAPEX	MM \$/y	155.6	133	150.5
- OPEX	MM \$/y	157.7	162.2	162.5
- GN added value	MM \$/y	/	/	-211
Total	MM \$/y	313.3	295.2	102
Unit Cost	\$/t	26.1	24.6 -6%	8.5 -67%

- Export terminal very simplified
- It could be installed in small places with berthing capacities or even other turret mooring
- No problem of safety linked to large refrigerated spheres
- Offshore connection is easier
- Less shut down to foresee as less mechanical equipment at both ends

- The cost of CO₂ shipping with **conventional** refrigerated scheme seems too important to implement a global possible scheme within an overall CO₂ value of 20-30 \$/t
- Solution with ambient temperature **unconventional gas** gives some advantages of simplifying terminals and then related environmental constraints
- But their costs, only slightly below the conventional one, remain too high **unless cost is offset by valorisation of stranded gas on way back, in the supercritical mode**

Then the most important point is to identify offshore reinjection structures with stranded gas resources with the same structure or nearby.

Thank you for your attention



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